



Flare Gas Mass Flow Metering Innovations Promise More Economical Choices

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INTRODUCTION

As the drive towards energy independence in the United States continues at full speed, oil and gas companies are turning to hydraulic fracturing to increase production. Increasingly stringent state and national regulations for flare gas in particular now require the installation of mass flow measurement instruments to measure waste and excess gases burned off as a result of the hydraulic fracturing process. For gas wells alone, the EPA estimates that the cost of compliance will rise to \$754 million per year by 2015.¹

Given the immense number of flares that are to be regulated, there is a need for more cost-effective mass flow measurement technologies. Multi-path ultrasonic flow meters have been widely used for flare gas measurement, but they are extremely expensive and have marked limitations. To comply with regulations, oil and gas companies need new flow meter alternatives that are accurate, durable, reliable and economical.

This paper reviews flare gas flow measurement challenges and describes how several recent innovations in thermal mass flow sensor technology gives end-users an alternative metering choice to consider. Of particular interest is four-sensor thermal technology coupled with an advanced math model algorithm that works in tandem with the American Gas Association's (AGA) compliant gas property database. In combination, these technologies allow the user to adjust the instrument and retain accuracy as flare gas compositions change in the field over time. The ability of this new breed of four-sensor thermal meter to adjust for changing gas compositions gives end-users a significantly lower cost alternative to four-path ultrasonic meters.



Background: Hydraulic Fracturing

Hydraulic fracturing is used to release oil and natural gas from wells drilled into reservoir shale rock formations called "shale plays". While fracturing itself is not new (first done in 1947), it is the perfecting of horizontal-drilling techniques that have made it economical to exploit these shale plays. The oil produced using these techniques and other new exploration technologies is poised to make the USA the world's largest producer of oil by 2020.²

The process of hydraulic fracturing releases large amounts of natural gas. While this is the objective in fracturing a natural gas well, some natural gas is inevitably released during the well completion (called flow back). Oil wells almost always produce natural gas ("associated gas") along with the petroleum. In many cases, it is uneconomical to process due to heavy contamination. Many of the newer fracturing discoveries do not have the pipelines, compressors and gas plant infrastructure to collect this gas. As a consequence, this gas is combusted, "flared off" or simply vented as-is. When all sources are considered, over 150 billion cubic meters are flared or vented globally every year. This is equal to 25% of the United States' natural gas consumption in 2012.³ Methane itself is a very potent greenhouse gas, while the carbon dioxide, soot and other contaminants in flared gas are also significant pollutants.

Flare Gas Measurement Challenges

In order to comply with state and federal regulations, oil and gas companies need to invest in mass flow measurement equipment to measure flare gas flowing to: the combustor, vented gas from storage tanks, gas used as fuel, and/or gas sent to the grid for sale. Each well has its unique and constantly changing characteristics that include depth, temperature, pressure, flow rate, soot content and changing gas composition. This makes accurate flare gas measurement very challenging. To comply with stringent state and federal regulations, engineers at oil and gas companies must assess which flow measurement technology yields the highest accuracy with the lowest installation and cost-of-ownership over the lifetime of the well.

The choice of flow measurement technology for flare gas measurement needs to perform under the following application challenges:

Wide Flow Rate Variations

Turndowns of up to 1,000:1 may be required.

Non-Uniform Flow Profile

Flare stacks generally have asymmetric and swirling flow.

Very Low Pressure with Variable Temperatures

Most flare headers operate at near atmospheric conditions. Gas temperature varies with well depth and reservoir characteristics.

Dirty Flares Versus Clean Flares

Many flares have significant amounts of dirt, hydrogen sulfide, wax, tar, and other paraffins that make for a dirty, sooty flame.

Maintenance Is Difficult and Costly

Roaring flames, difficult access and regulatory requirements make flares difficult to service.

Wide Gas Density Variations

Flare gas composition, and thus the density of flare gas varies over the lifetime of the flare. Traditional flow meters cannot successfully manage the changes in flare gas composition.



As seen in Table 1 (Flare 1), the molecular percentage of hydrogen changes from 86.18% to 48.77%, and methane changes from 5.93% to 3.52% over a year of operation. Faced with such changing flare gas composition, a typical total flow measurement error can be in the 5% to 10% range and could be as high as 20% in applications with widely varying compositions. Correcting measured linear velocities to actual mass flow rates can be problematic if the molecular weight of the waste gas varies by more than 20% from the molecular weight of the meter's calibration gas.

| Flare Gas Composition Variability: Flare 1 | | | | |
|--|--------|--------|--|--|
| COMPONENT | MOLE % | MOLE % | | |
| hydrogen | 86.18 | 48.77 | | |
| methane | 5.93 | 3.52 | | |
| ethane | 0.81 | 0.26 | | |
| ethylene | 0.02 | 0.01 | | |
| propane | 0.34 | 0.14 | | |
| propylene | 0.00 | 0.01 | | |
| n-butane | 0.11 | 0.05 | | |
| i-butane | 0.11 | 0.06 | | |
| cis, 2-butylene | 0.16 | 0.06 | | |
| trans, 2-butylene | 0.17 | 0.06 | | |
| isobutylene | 0.12 | ND | | |
| 1,3-butadiene | ND | ND | | |
| n-pentane | 0.03 | 0.08 | | |
| i-pentane | 0.05 | 0.05 | | |
| pentenes | ND | ND | | |
| C ₆ + | 0.01 | 0.01 | | |
| CO | 0.02 | 0.04 | | |
| N ₂ | 4.99 | 45.80 | | |
| 0 ₂ | ND | ND | | |
| co ₂ | 0.06 | 0.04 | | |
| hydrogen sulfide | 0.24 | 0.35 | | |
| water vapor | 0.68 | 0.70 | | |
| Totals | 100.00 | 100.00 | | |

Table 1. Examples of Flare Waste Gas Compositions—Constituents of Interest and Variability over 1 Year⁴



Many Meter Choices—Few Good Solutions

Over the last five years, multi-path transit-time ultrasonic meters (typically four-path) have been used for flare gas measurement. Given the flare gas measurement challenges they face, multi-path ultrasonic flow meters perform reasonably well. With multi-path ultrasonic flow meters, speed of sound through the flare gas is directly related to its density. This makes flare gas measurement independent of changing gas composition and facilitates mass flow measurement.

Because the sensors are non-intrusive (not exposed directly to the flare gas), they have been used in some installations to measure dirty, wet gas without gumming up mechanical parts, resulting in lower maintenance costs. However, in some applications, dirt, wax, tar, and paraffin in the flow causes internal erosion or build-up of material on the inner wall of the pipe. Since multi-path ultrasonic meters are built into in-line pipe sections, called spool pieces, the entire meter must be removed to clean them. This degrades the flow measurement accuracy without obvious indicators. Susceptibility to the effects of flow profile, especially swirl, will also cause degraded accuracy.

Multi-path ultrasonic meters are distinguished by the number of paths they use to compute the flow rate. Multiple paths enable more precise calculation of the gas velocity and the speed of sound (and thus density), but each set of paths substantially increases the cost. Cost also increases with the size of the spool piece. This can cost oil and gas companies over \$15,000⁵ for a four-path ultrasonic flow meter. This cost is several times more than the traditional flow meters (depending on the technology) listed in Table 2 (next page).

Other technologies listed in Table 2, like averaging pitot tubes and insertion turbine meters, have poor performance for measuring flare gas. These devices measure volumetric flow, not mass flow, which is the desired measurement. They require a clean flare gas with constant gas composition. Additionally, multivariable mass vortex meters successfully measure low pressures of flare gas, but they need to know the gas composition for accurate measurement.





| Comparison of Flow Technologies Based on Performance Factors | | | | | | | | |
|--|----------------------------------|---|---|---|--|----------|--|--|
| | HIGH & LOW FLOW (TURNDOWN) | LOW PRESSURE | DIRTY FLARES | VARYING COMPOSITION | FLOW PROFILES | COST | | |
| Averaging Pitot Tubes | | | | | | | | |
| and the start | poor 10 to 1 | poor ∆P device | poor Prone to clog | poor Volumetric | good Averages across pipe | \$2,000 | | |
| Insertion Turbines | | | | | | | | |
| CATE | poor 10 to 1 | fair Minimum velocity | poor Prone to clog | poor Volumetric | poor Point measurement | \$1,000 | | |
| Insertion Vortex | poor Minimum velocity | good Multivariable | fair Sensor head can plug, but is fairly large | poor Must know gas composition | poor Point measurement | \$3,000 | | |
| Insertion Thermal | good 1,000 to 1 | fair Must be calibrated at operating pressure | poor Clean flares only | poor Must know gas composition | good Point measurement | \$2,500 | | |
| Ultrasonic | fair 100 to 1 | excellent Not affected | excellent External to pipe | good Infers density from speed of sound | fair Signal accross pipe | \$15,000 | | |
| QuadraTherm | excellent 2,000 to 1 | excellent Multivariable | fair Sensor head can plug, but is fairly open | good Four compositions on board, any other can be uploaded in field | fair Point measurement, but Reynolds number correction built in | \$3,000 | | |

Table 2. Comparison of Flow Technologies Considered for Flare Gas Metering



Four-Sensor Thermal Mass Flow Meters

Traditional thermal flow meters have limitations in flare gas measurement because they can't accurately measure changing gas composition without factory recalibration. Recent innovations in thermal mass flow sensor technology have removed this barrier to market entry. Four-sensor thermal mass flow meters now have the ability to adjust for changing flare gas compositions in the field over time. This new four-sensor thermal meter gives end-users a lower cost alternative to four-path ultrasonic meters in flare applications.

Improved Accuracy Specification

With four-sensor thermal sensor technology, as seen in Figure 1, accuracy specifications are comparable to four-path ultrasonic meters at a much more economical price. Pioneered by Sierra Instruments, Inc., in Monterey, California, four-sensor thermal has +/-0.75% of reading accuracy for insertion-probe versions (far better than the 2.0% of reading previously possible with traditional thermal). The in-line version of the instrument improves on that with +/-0.5% of reading accuracy.



Figure 1. QuadraTherm® Four-Sensor Design by Sierra

Field Composition Changes, Now Possible

For the first time, four-sensor technology can compete with multi-path ultrasonic meters due to its ability to compute the mass flow rate of any gas composition. Hyper-fast microprocessors run flow-measurement algorithms to compute the mass flow of any gas composition. The microprocessor takes the inputs from the four sensors and solves the First Law of Thermodynamics (Heat Energy In = Heat Energy Out) for each data point.



In thermal mass flow meters, the composition of the gas is required. Flare gas composition sampling depends on the wellhead and typically done once every three months. Once the flare gas composition is known, operators can create, name, store and upload new gas compositions to the four-sensor meter (See Figure 2). Accuracy is maintained without sending the meter back to the factory for costly recalibration.

The meter itself stores four gas compositions. Operators can access the software's gas library, which is password protected to keep proprietary gas mixtures secure. This gas library contains all AGA compliant gas properties needed to make the algorithmic gas mass flow rate calculations.



Figure 2. Smart Interface Portal—QuadraTherm Embedded Gas Composition Management Tool

Cost Savings

It was clear from the comparison of flow technologies for flare gas metering in Table 2 that both thermal and ultrasonic are the preferred choices. At this point, it is a good time to review costs and overall cost of ownership. Table 3 gives a five year cost of ownership example comparing a traditional 6.0 inch (150 mm) long two-sensor insertion-probe thermal mass meter inserted into a 4.0 inch (100 mm) flare header, with an inline 4" (100mm) four-path inline ultrasonic meter, and a 6 inch (150 mm) long four-sensor insertion-probe thermal mass meter inserted into a 4" (100 mm) flare header. The four-path ultrasonic meter averages \$15,000 (Flow Research, Inc. 2008 Study), while the four-sensor thermal insertion-probe meter averages \$3,000. Insertion-probe thermal meters also accommodate larger pipe applications up to 72 inches (2m) with a single 0.75 inch (19mm) insertion point.



Ultrasonic meters only have in-line flow body configurations, and the cost increases exponentially with pipe size and number of paths.

Using the Table 3 data, let's assume that a typical customer has 150 flare gas measurement points. When the composition changes five times over the life of the wellhead, costs add up. Using four-path ultrasonic metering would cost \$2,475,000, but the instrument would be unaffected by gas composition changes. In contrast, the four-sensor thermal meter would be much less expensive at \$562,500, even though periodic field adjustments of the four-sensor thermal meter would be required.

If you take a more macroeconomic view on the industry and make the reasonable estimate of 30,000 new flares per year that need measurement, annual ultrasonic metering costs are pushed to \$495 million. Under these same assumptions, four-sensor thermal would cost much less at \$112 million. These cost estimates support the need for alternative, lower cost metering choices for this tough application. In the absence of lower cost options, energy costs will increase over the long-term as high metering costs are pushed to the consumer in the form of higher prices.

| Flow Meter Cost-of-Ownership Comparison | | | | | | | |
|---|--|---|---|--|--|--|--|
| | 6 inch (150 mm) TRADITIONAL 2-SENSOR THERMAL INSERTION-PROBE MASS FLOW METER | 4 inch (100mm) INLINE 4-PATH ULTRASONIC FLOW METER | 6 inch (150 mm) 4-SENSOR THERMAL INSERTION-PROBE MASS FLOW METER | | | | |
| Instrument Initial Cost | \$2,500.00 | \$15,000.00 | \$3,000.00 | | | | |
| Installation | \$ 500.00 | \$ 1,500.00 ² | \$ 500.00 ³ | | | | |
| Calibration 1 | \$ 850.00 ¹ | 00.004 | \$ 50.00 ⁵ | | | | |
| Calibration 2 | \$ 850.00 | 00.00 | \$ 50.00 | | | | |
| Calibration 3 | \$ 850.00 | 00.00 | \$ 50.00 | | | | |
| Calibration 4 | \$ 850.00 | 00.00 | \$ 50.00 | | | | |
| Calibration 5 | \$ 850.00 | 00.00 | \$ 50.00 | | | | |
| Total | \$7,250.00 | \$16,500.00 | \$3,750.00 | | | | |

Table 3. Example of Five Year Cost-of-Ownership Comparison Between Traditional and Four-Sensor Thermal Mass Flow Meters Versus Multi-Path Ultrasonic Flow Meters

Table 3 Notes:

Assume a 4 inch (100mm) flare header and gas composition that has changed 5 times over 5 years where it was dramatic enough to warrant instrument adjustment.

- ¹Cost to remove instrument, ship back to factory, recalibrate to new gas composition, return and reinstall. Cost of process measurement downtime not calculated
- ² Must shut process, cut pipe to install inline ultrasonic flow meters. Cost of process measurement downtime not calculated
- ³ Single 6 inch (19.1mm) insertion point, can be hot-tapped
- ⁴No need for removal from pipe or adjustment
- ⁵ Assume cost of 30 minutes at \$50 labor cost each time the instrument is adjusted for new gas composition via field software interface.



Summary and Conclusions:

Oil and gas companies may potentially lose thousands of dollars a day if they are not in compliance with local, state and federal regulations. And flow metering costs will drive energy prices up as they are passed to the consumer at the gas pump. In addition, as infrastructure is developed, gas that is

now flared will eventually be sold to the national distribution network, turning a current liability into a future asset.

While multi-path ultrasonic flow meters are widely used today, end-users now have an alternative. Primarily due to the significantly lower cost of ownership, four-sensor thermal mass flow technology is poised to become a highly attractive alternative. The ability to adjust the instrument in the field in response to changing flare gas compositions over time and the extremely high accuracy of these devices offer oil and gas companies a compelling alternative to multi-path ultrasonic meters.

Acnowledgements

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Figure 3. 4-Sensor Insertion-Probe QuadraTherm Mass Flow Meter by Sierra